

Water Treatment at AES, Maritza East I TPP

An Overview

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General Data

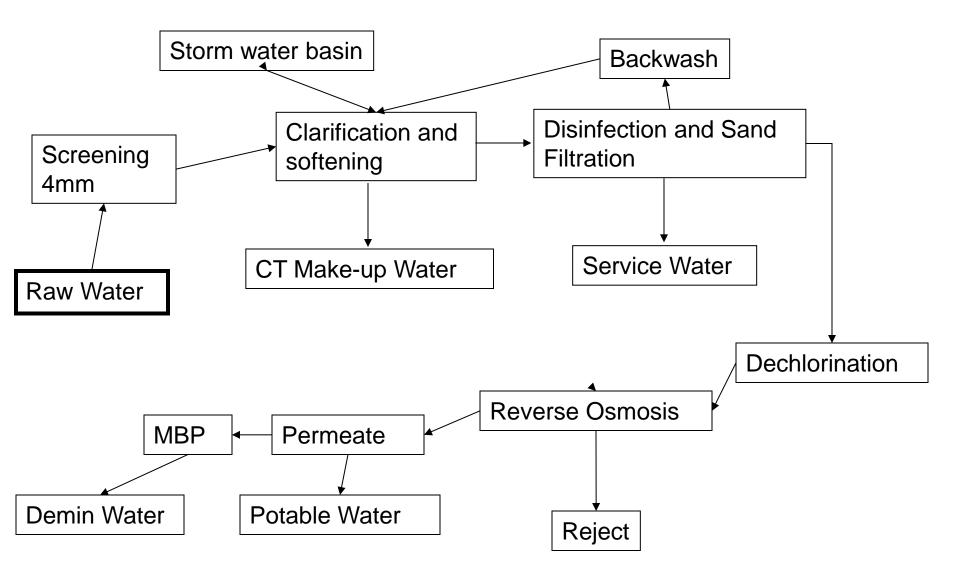
- Lignite Fired power station 2x300 MW Alstom turbines-generators
- 2 Alstom Boilers generating ~ 1022 ton/hour steam @ 544 °C/177 bar each (Maximum Load) with ESP and FGD installations
- Natural draft Cooling tower (61200 m3/hr flow, 16000 m3 system volume, 3-6 cycles of concentration)
- 2 x Condensers with stainless steel (DIN 1.4301) tubes

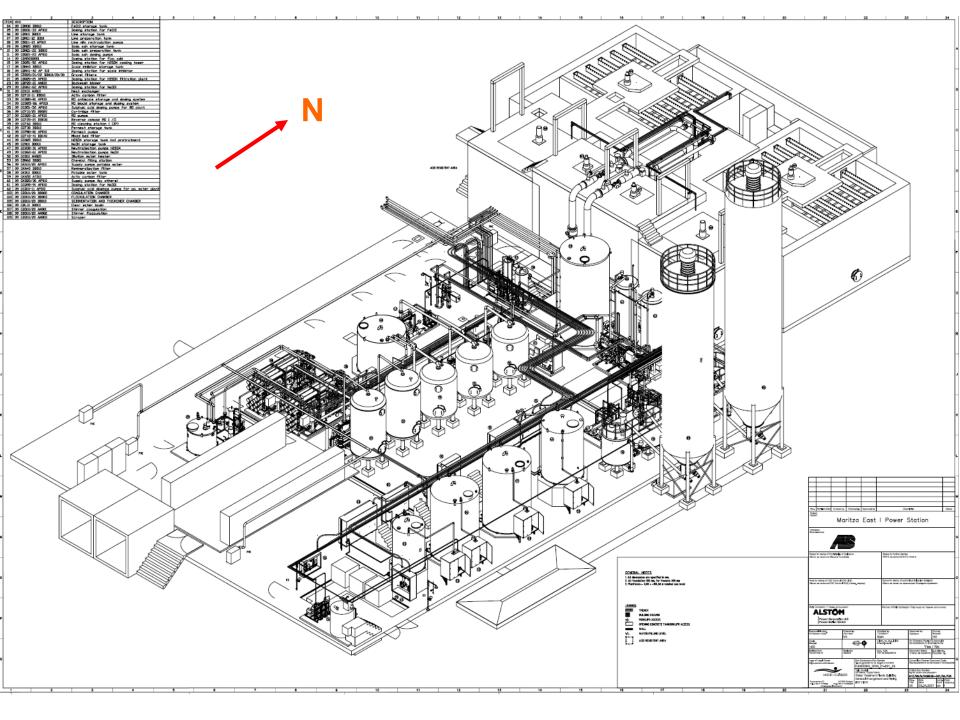
EHS

- Zero Liquid Discharge: All waste water streams are recycled.
- Minimal chemical use
 - 96% H2SO4:
 - * Before RO technology: 4670 ton/year
 - * After RO technology: 875 ton/year
 - 50% NaOH:
 - * Before RO technology: 11518 ton/year
 - * After RO technology: 73.6 ton/year
- No Harmful chemicals (no Hydrazine)
- All chemical containers bunded and chemical filling is designed with overfill protection
- Safety showers and PPE provided

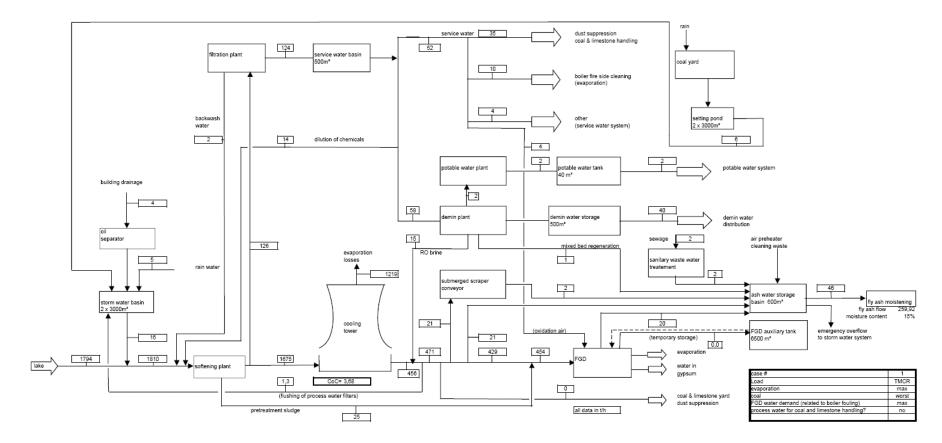


Block Diagram for WTP





Water balance



Impurities

- Raw water is brackish (TDS ~ 1000 mg/L), scaling due to hardness (10-14 meq/L), TOC is high (5-30 mg/L due to humics and chlorophyll), sulfate is high, Silica, Barium/Ca sulfate is a potential scalant
- Raw water is surface water and hence has bacteria/phytoplankton/algae/fish/mussels (potentially)
- Raw water has turbidity (suspended solids, colloids) / color

Types of Water (Produced and Waste Streams)

- Raw Water (Rozov Kladenets)
- Main Cooling Tower Make-up Water (clarified and softened)
- Service Water (pH adjusted, disinfected and filtered)
- Process Water (CT Blow-down Water)
- RO Permeate (demineralized service water 5 mg/L TDS)
- Potable Water (remineralized, A/C treated, disinfected)
- Demin Water for Boiler (RO permeate deionized using MBP's)
- Regeneration waste (from regenerating the MBP's)
- RO reject (recycled into CT make up water)
- Ash Water (FGD blowdown water, neutralization waste, RAPH cleaning waste, treated sanitary water, SSC blowdown)
- Storm water (recycled into clarifier)
- Coal storage yard drain water (recycled into storm water basin)
- Sanitary waste water (treated using STP and used for ash moistening)
- Oil-separator effluent (recycled into Storm water basin)

Water Treatment Systems

- Clarifiers (FLOCOPAC) for Raw Water Treatment with capacity of 2200 m3/hr: Coagulation, flocculation, chemical softening and settling with recycling of sludge produced into FGD process. Reduce TSS down to 10 mg/L and Hardness down to 1 meq/L
- Sodium hypochlorite dosing (for service water and CT)
- Gravel/Sand Pressure Filters (total capacity = 133 m3/hr) reduce TSS to less than 1 mg/L
- Active Carbon Filters (pre-treatment for RO)
- 5 micron filters (pre-treatment for RO)
- Three-stage Reverse Osmosis Units x 2 / CIP Station
- MBP
- Closed Cooling Water System Chemical Feed System
- Ball cleaning system/self-cleaning filters for the condenser

Water Treatment Systems

- Boiler feed water and condensate treatment for ~ 1000 tons/hr steam per boiler (Ammonia + backup NaOH)
- Remineralization filter (CaCO₃) for potable water
- Oil Separators (Boiler and Turbine area)
- Package Sewage Treatment Plant (Fixed film activated sludge process)
- Storm Water Basin for rain water (which is collected and reused) and Settling basin for coal yard drainage water (the latter is recycled in storm water system)

Processes/Chemicals

- FeCl₃ as coagulant, anionic Polyacrylamide as flocculant and Na₂CO₃/Ca(OH)₂ for chemical softening
- NaOCI as disinfectant for service water and Main CT water
- Anti-scalant/H₂SO₄ for the cooling tower
- Corrosion inhibitor for fire-fighting system
- NaOH and H₂SO₄ for regeneration of the MBP
- RO antiscalant and cleaning chemicals: acid clean (citric acid based) and base clean (caustic + surfactant)
- DBNPA for the RO
- SBS for preservation of membranes
- Caustic Soda + Ammonia for WSC

Raw Water Pumping Station

- Two pumps 100% each
- Traveling Band Screen
 (Eimco Water technologies)





Coagulation, Flocculation, **Precipitation and** Settling

FLOCOPAC

FLOCOPAC

Theoretical Aspects **Functional** Views Type of Construction

Explanation

- Coagulation Destabilisation of colloidal suspension by addition of chemical reagents (iron III chloride, aluminium sulphates etc.) by nullifying the repulsive forces
- Flocculation Agglomeration of the neutralized colloids into flocs by adding of flocculant (organic polymer)
- Precipitation/Settling Chemical precipitation means formation of insoluble compounds by action of appropriate reagents → Elimination of Calcium, Magnesium and Silica by Lime Softening. Settling means settling of flocs by action of gravity.

Water Quality

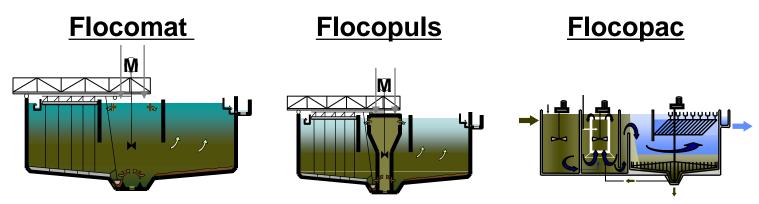
- TSS before: 20mg/L (65 in worst case)
- TSS After: < 10 mg/L
- Hardness Before: 10 meq/L (14 in worst case)
- Hardness After: < 1 meq/L

Explanation

Settling units with sludge re- circulation, sludge blanket units, plate settling and granular contact units

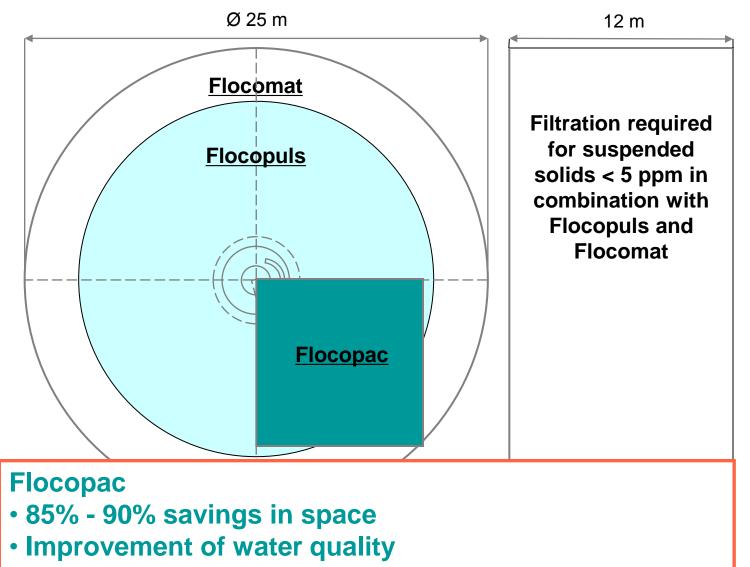
- Sludge re- circulation unit : FLOCOMAT
- Sludge blanket unit : FLOCOPULS
- High efficiency plate type unit with contact sludge upflow reactor
 : FLOCOPAC

Comparison

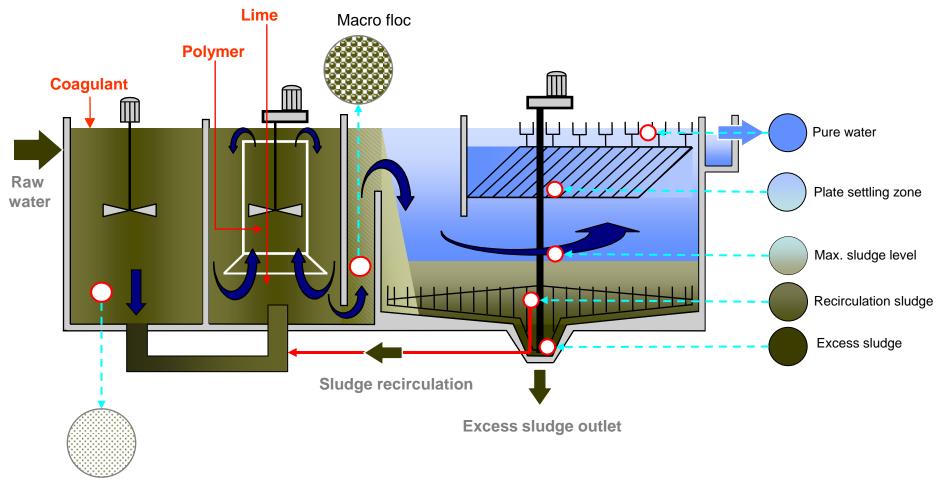


| •Upflow velocity | 1,5 – 1,8 m/h (Flocc) 2,8 – 3,5 m/h (Decarb) | 2,0 – 2,5 m/h (Flocc) 3,0 – 5,0 m/h (Decarb) | 20-25 m/h (Flocc) 30-35 m/h (Decarb) |
|-----------------------------------|---|---|---|
| Solids outlet | < 10 | 5-10 | < 2 |
| •Space requirement | High | Medium | Low |
| •Sludge concentration | Low | Medium | High |
| | | | |

Comparison Space Requirements Example: Flow rate approx. 1.500 m³/h

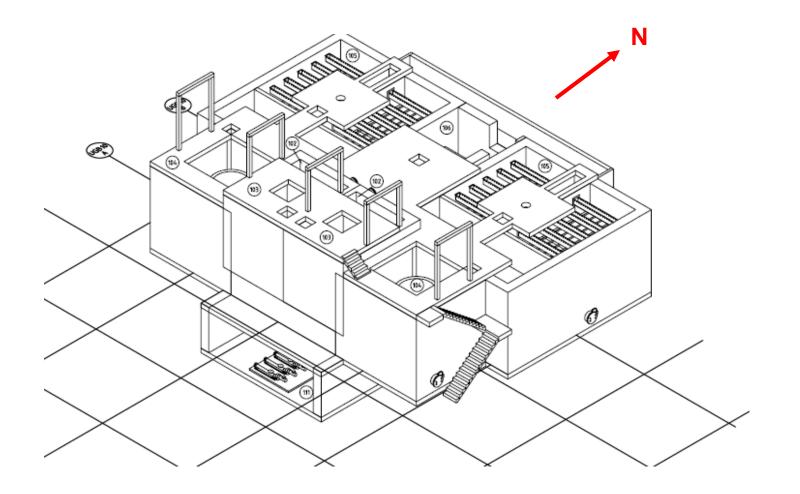


FLOCOPAC Functional View

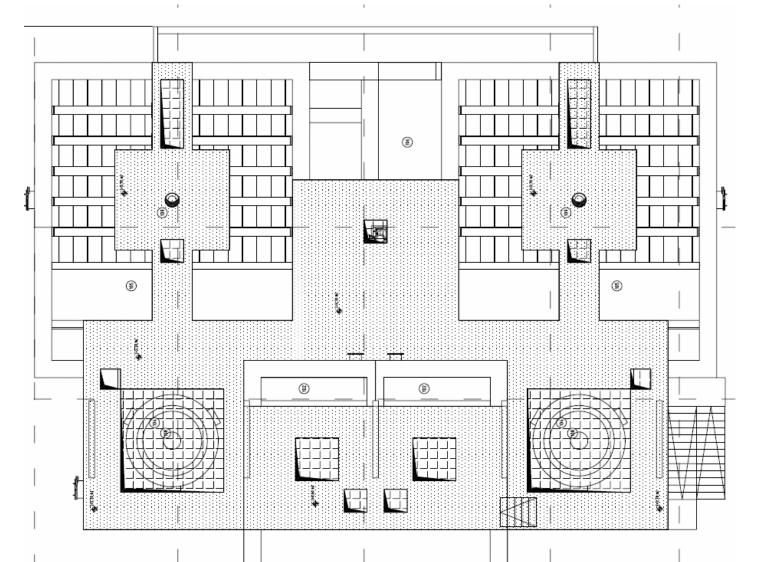


Micro floc

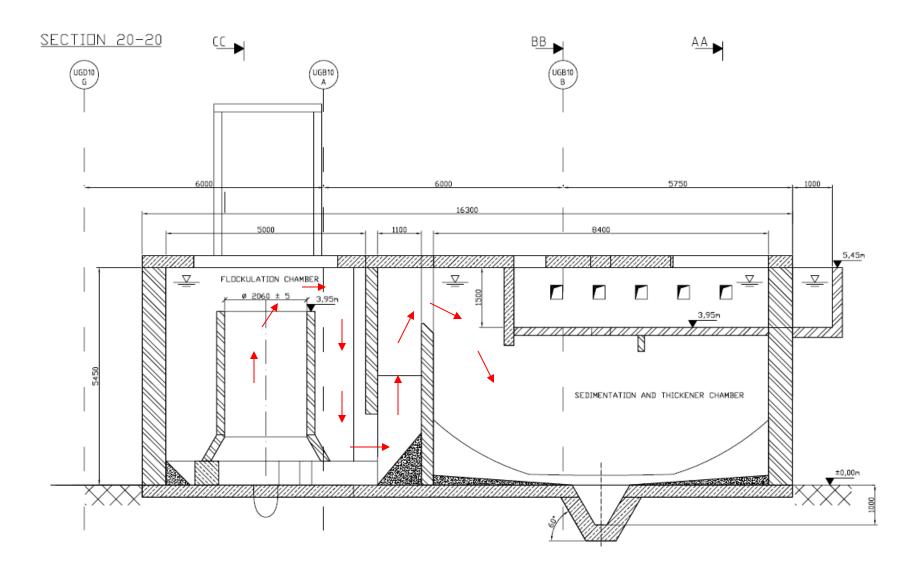
FLOCOPAC Isometric View



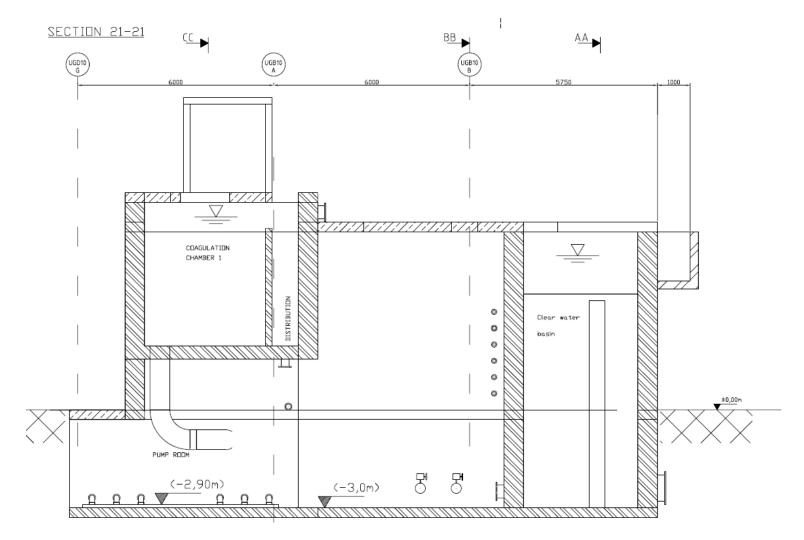
Arrangement (Top View)



FLOCOPAC Sectional Views - I



FLOCOPAC Sectional Views - II



FLOCOPAC Scraper



Clear Water Channels

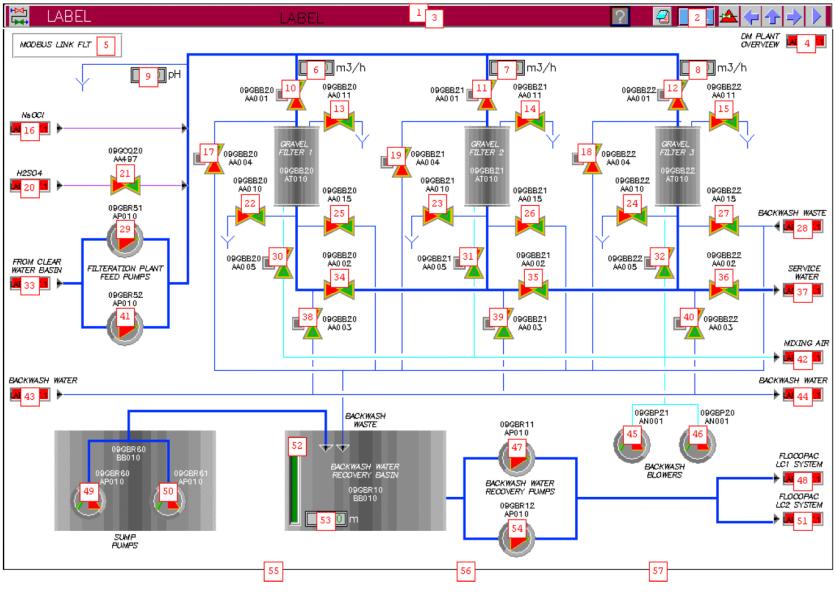


Lamella Modules

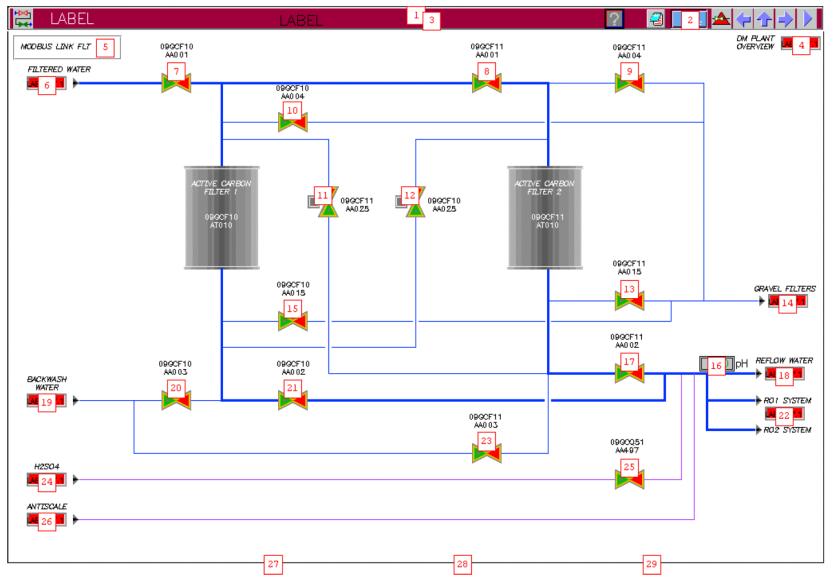




Gravel Filters (TSS < 1 mg/L)

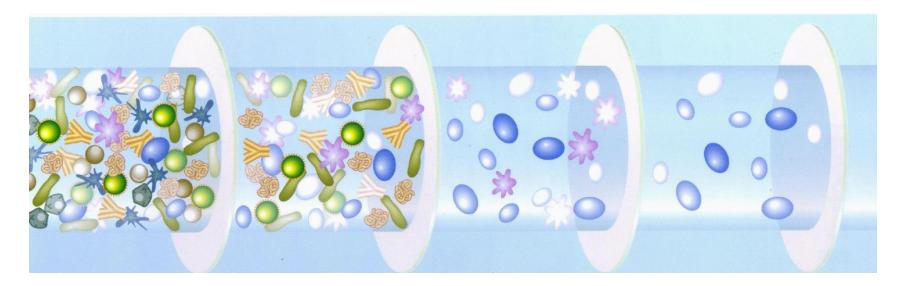


AC Filters



Reverse Osmosis

Membrane Separation



Mikrofiltration > 0,1 μm Ultrafiltration 0,1 - 0,01 µm

Nanofiltration 0,01 - 0,001 μm **RO**< 0,001 μm

- lons

- turbidity

- Suspended solids
- algae

- Colloidal substances

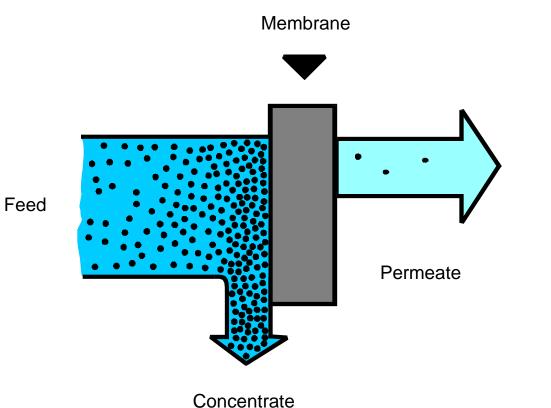
- Micro organism
- Organics
- Pesticides
- CaSO4

Reverse Osmosis

- Membrane solids separation technology
- Pressure driven process through a semipermeable membrane
- Retention of salts, organics (down to 100 amu) and micro-organisms
- Cross-flow operation mode
- Continuous process

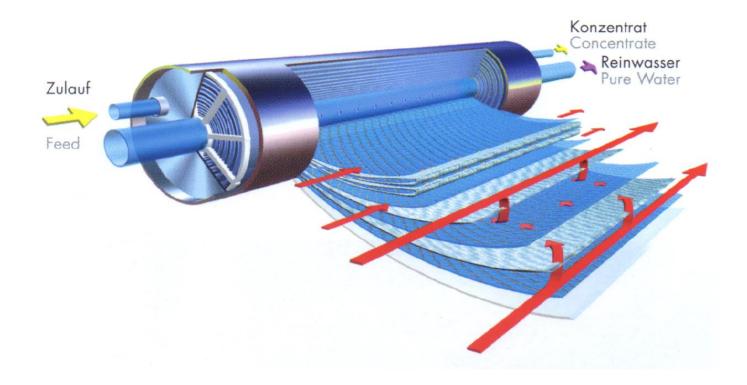


Principle of RO



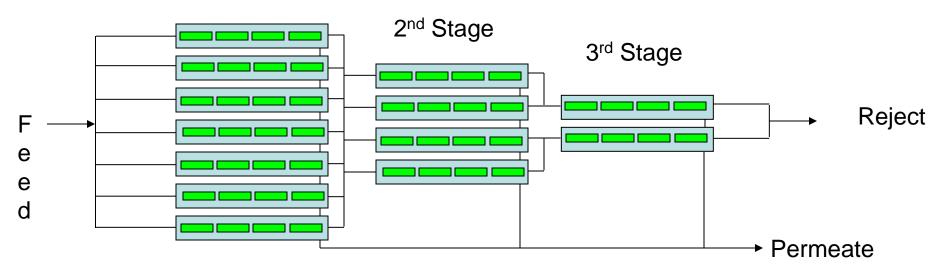
- Cross-flow filtration for continuous desalination
- Separation of feedwater into concentrate and permeate
- Average concentration factor 4-5

Reverse Osmosis Modules



R.O. Configuration at AES ME1

• 7-4-2 Concentrate Staging Configuration



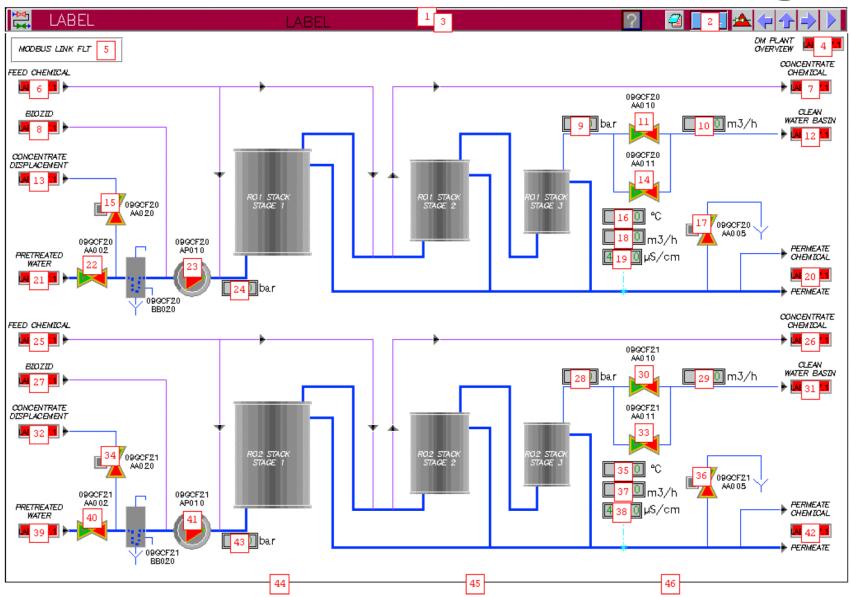
1st Stage

52 membrane elements in each train

RO At ME I



ALSPA Process Monitoring



RO Membrane Fouling/Deterioration

- Scale
- Colloids
- Oxidants
- Color
- Bacteria
- High/Low pH
- Sudden Pressure
- Organic solvents

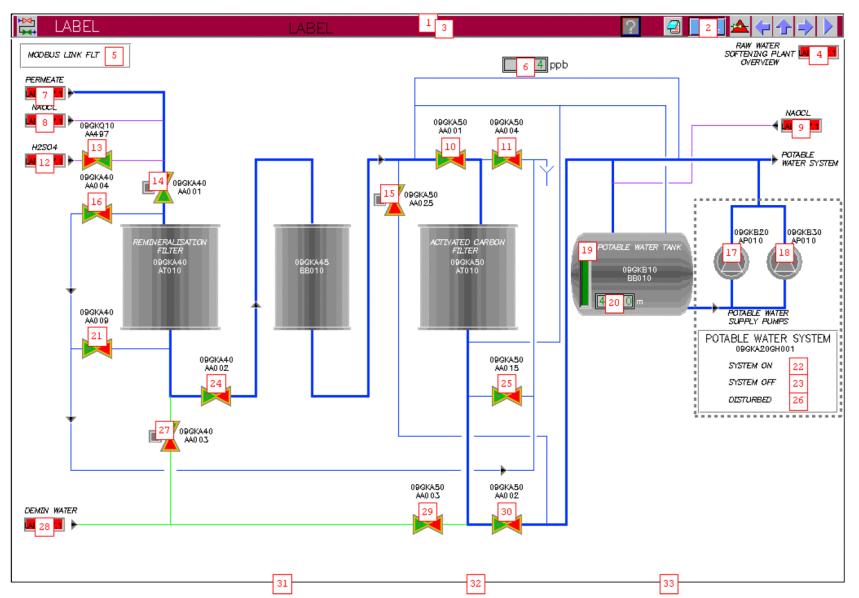
RO CIP



Monitoring the RO

- Ionic composition (weekly)
- Alkalinity (daily)
- Hardness (daily)
- Chlorine (daily)
- T, pH (per shift)
- Conductivity, SDI (per shift)
- TOC, Color (daily)
- Bacteria count (every 3 days)
- Silica (weekly)
- Humic/Fulvic acid (weekly)
- H2S (weekly)
- Boron (daily)
- Oil and Hydrocarbons (weekly)

Potable Water Treatment

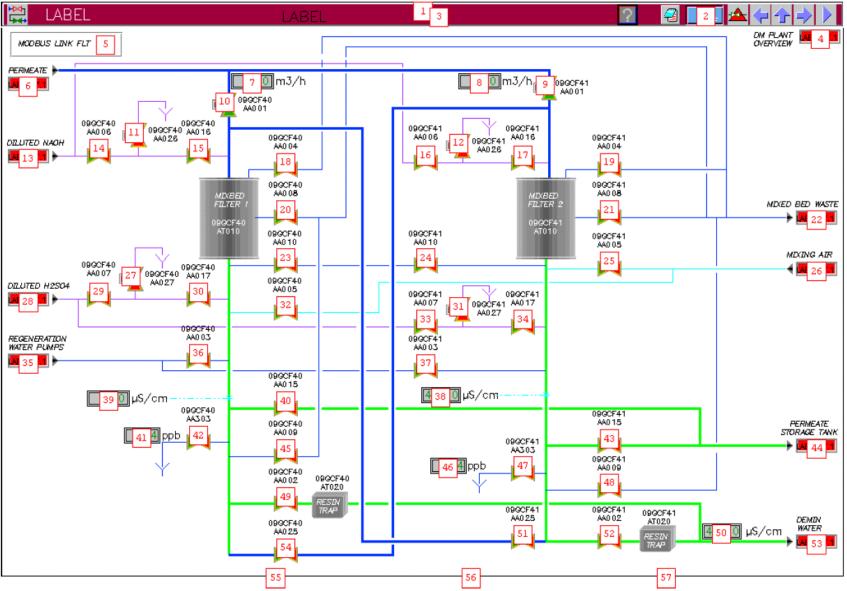


Mixed Bed Polisher

Mixed Bed Polisher

- Two vessels with 1-2/2-1 operation
- Strong cation and strong anion Rohm and Haas Amberlite (Amberjet 1200 H and Amberjet 4200 CI) resin.
- Regeneration with H₂SO₄ and NaOH every ~ 48 hours.
- Online monitoring of Conductivity and Silica

MBP at ME 1 WTP



Minimum Water Quality for Demineralized Water

- Total Dissolved Solids (TDS) < 0.025 mg/L (Conductivity < 0.08 µS/cm = 12.5 MΩ.cm resistivity)
- Silica as $SiO_2 < 0.01 \text{ mg/L}$
- Total Organic Carbon (TOC) < or = 0.3 mg/L
- D.O. guarantee at Economizer inlet: 10 ppb (without hydrazine)

Dosing Regime for WSC

- Based on VGB-R 450 Le
- No Copper materials hence pH can be higher than 9.3
- O₂ level of 10 ppb at econ. inlet w/o Hydrazine
- Dosing facilities for solid alkalizing agent (dosed at econ. inlet according to pH in SD) and ammonia (downstream condensate extraction pumps according to pH at econ. inlet)

Quality Requirements – Feed Water

| Parameter | Unit | Ν | A1 | |
|--|-------|-----------|--------|-----|
| рН | - | 9,2 – 9,4 | 9,2 | 9,8 |
| Conductivity (only valid for ammonia dosing) | µS/cm | 4,3 – 8,6 | 4,3 | 18 |
| Acid conductivity | µS/cm | < 0,10 | 0,2 *) | |
| Oxygen (O2) | µg/kg | 5 - 20 | 2 | 100 |
| Silica (SiO2) | µg/kg | < 5 | 20 | |
| Iron (Fe) total | µg/kg | < 10 | 30 | |

Quality Requirements – Steam Drum

a) AVT (Alkaline Treatment)

| Parameter | Unit | Ν | A1 |
|-------------------|-------|---|-----|
| рН | - | pH is controlled by pH of the feed water (pH of feed water to be > 9,5) | |
| Acid conductivity | µS/cm | < 1 | 1 |
| Silica (SiO2) | µg/kg | < 75 | 300 |

b) Caustic Soda dosing to HP drum

| Parameter | Unit | N | A1 | |
|-------------------|-------|-----------|-----|-----|
| рН | _ | 9,4 – 9,6 | 9,3 | 9,7 |
| Conductivity | µS/cm | 6 – 10 | 5 | 12 |
| Acid conductivity | μS/cm | < 30 | 30 | |
| Silica (SiO2) | µg/kg | < 75 | 300 | |

Quality Requirements – Live Steam

| Parameter | Unit | N | A1 | |
|---|-------|--------|--------|--|
| Acid conductivity | µS/cm | < 0,10 | 0,2 *) | |
| Silica (SiO2) | µg/kg | < 5 | 20 | |
| Sodium (Na), if boiler water treatment AVT or caustic | µg/kg | < 2 | 5 | |
| Sodium (Na), if boiler water treatment with phosphate | µg/kg | < 5 | 10 | |
| Iron (Fe) total | µg/kg | < 5 | 20 | |
| Copper (Cu) total | µg/kg | < 1 | 3 | |

*) Higher values may be defined if the increase of acid conductivity can be attributed to carbon dioxide from air inleakage but organic decomposition products can be excluded

Monitoring

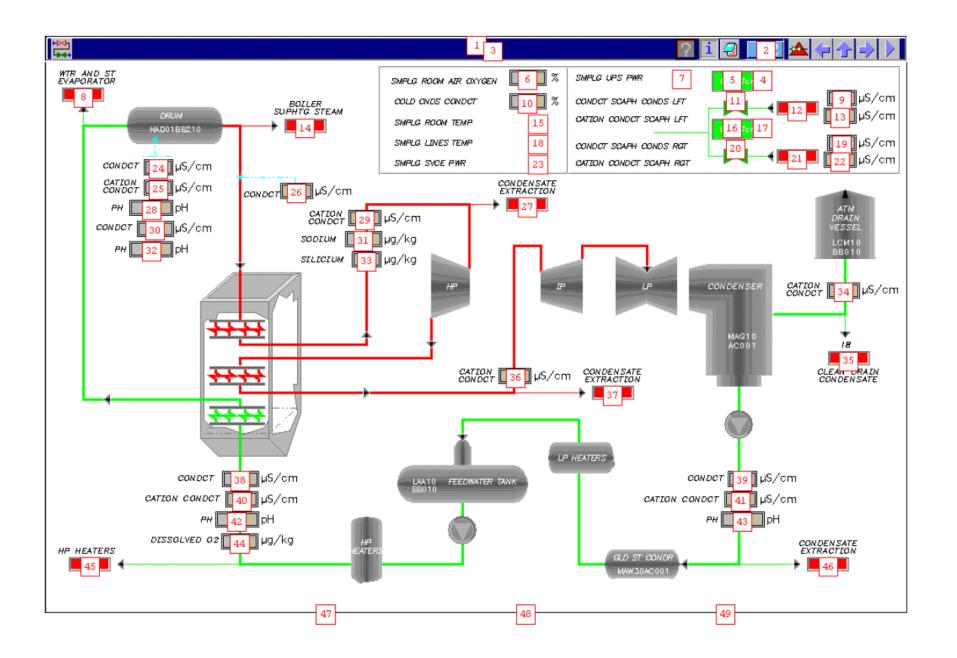
- Water/Lignite/FGD analysis lab for grab samples:
 - Inorganics (heavy metals, phosphates, nitrates, chlorides, etc.), pH, COD, turbidity, hardness, chlorine, ammonia, SDI
 - Lignite: LHV, ash, moisture, volatiles, C/S-content, sieve analysis and boiler/ESP by-products
 - FGD raw materials/byproducts
- Online monitoring (for clarifier, RO, MBP, WSC and CT): pH, turbidity, sludge density, Na, Silica, DO, Conductivity, Cation Conductivity, Chlorine.

Online Monitoring WSC

| Sampling point | parameter | Measuring range | Remarks |
|--|---------------------|---|--|
| Condensate after condensate extraction pumps | Direct conductivity | 0 – 80 μS/cm | |
| | Acid conductivity | 0 – 2 μS/cm | |
| | Calculated pH | 7 – 12 pH | No analyser, calculated from acid conductivity and direct conductivity |
| | (Dissolved oxygen) | (0 – 400 μg/l O ₂) | Analyser for measurement for feed water at economizer inlet may be manually interchanged to this sampling point |
| Feed water, at economiser | Direct conductivity | 0 – 80 μS/cm | |
| inlet | Acid conductivity | 0 – 2 μS/cm | |
| | Calculated pH | 7 – 12 pH | No analyser, calculated from acid conductivity and direct conductivity |
| | Dissolved oxygen | 0 – 400 µg/l O ₂ | (Shared analyser, may be used also for condensate measurement after condensate extraction pumps |
| | Hydrazine | 0 – 20 μg/l N ₂ H ₄ | |
| Main steam | Acid conductivity | 0 – 2 µS/cm | |
| | Silica | 0 – 40 μg/l O ₂ | |
| Saturated steam | | | Sample line interconnected to main steam sampling point to use analysers installed at this sampling line |

Monitoring WSC

| Sampling point | parameter | Measuring range | Remarks |
|----------------------|-----------------------------------|-----------------|--------------------|
| Reheat steam | Acid conductivity | 0 – 2 µS/cm | |
| Boiler drum water | Acid conductivity, continuously | 0 – 150 µS/cm | Split range output |
| | Direct conductivity | 0 – 150 µS/cm | |
| | pH measurement | 4 – 12 pH | |
| Cold condensate tank | Direct conductivity, continuously | 0 – 80 µS/cm | |
| Condensate return | Acid conductivity | 0 – 2 µS/cm | |



Automation/PLC

- PLC system controls all automation in water treatment plant
- Opening/closing of valves for various sequences and turning pumps on/off
- Flow control for chemical dosing pumps
- Process DCS Simulation (ALSPA system) displays process parameters in Main Control Room (HMI)

Main Equipment

- +GF+ PP and PVC piping and tanks
- Steel tank for H2SO4 and steel pipes for steam
- Gemu/Georg Fischer butterfly/membrane valves
- Toray RO Membranes
- KSB, Sterling, Apollo, Munsch, Seepex and Wilo pumps

sarco

- Grundfos Chemical dosing pumps
- Spirax Sarco heat exchangers and steam valves
- Nord/KSB motors spiral
- Kaiser blowers
- Endress hauser flow meters/LI's
- Jumo electrodes (pH/Conductivity)



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